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Energy, Utilities and CO2 Emission Management with AVEVA RTO at REPSOL

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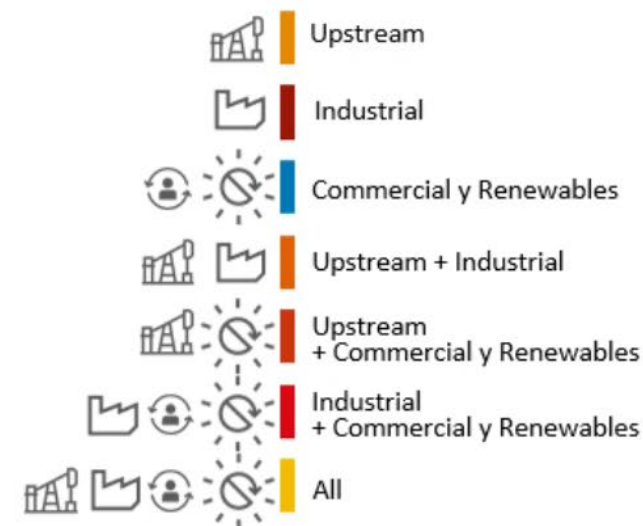
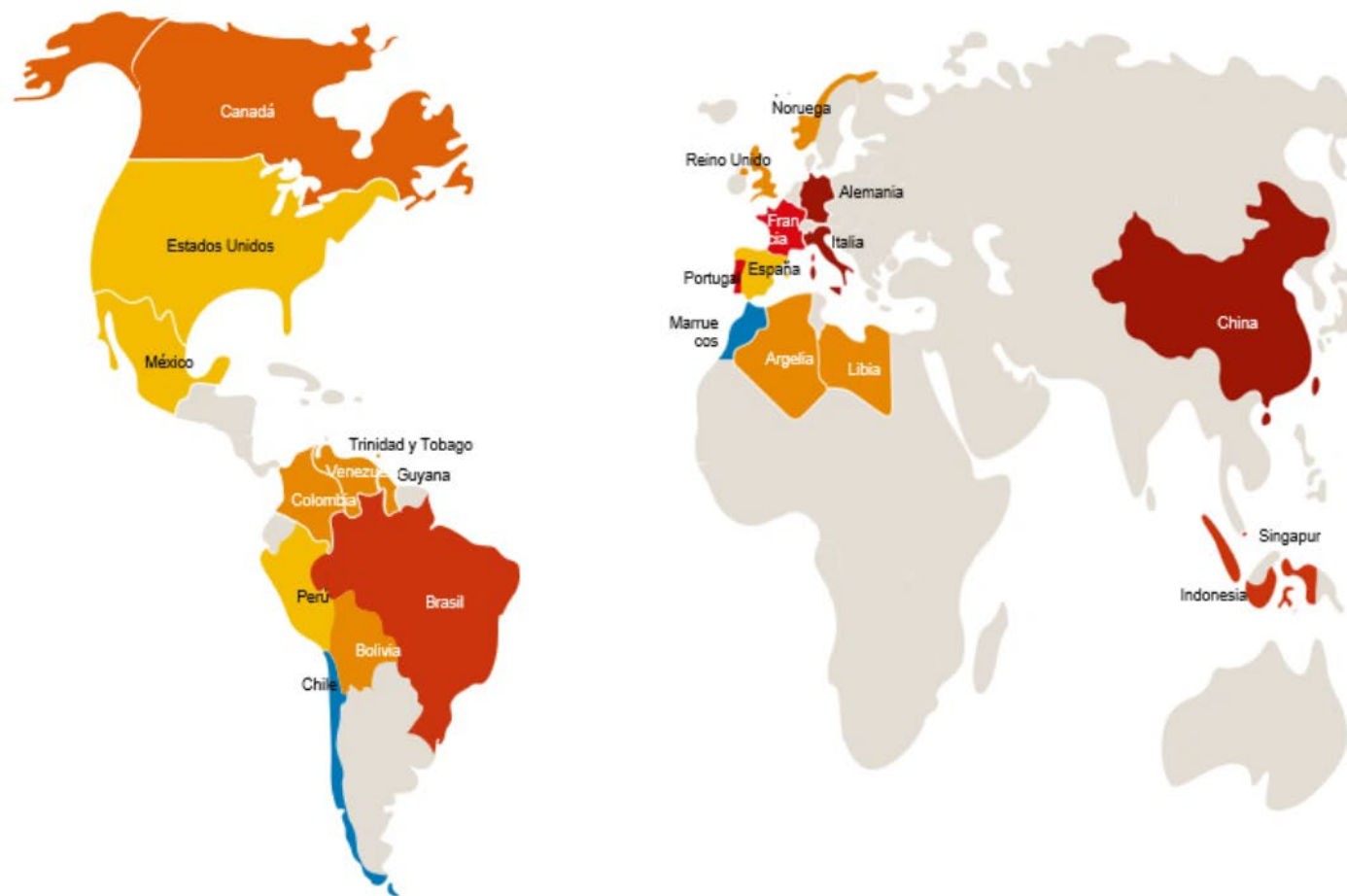
Agenda

- Introduction
- Problem Description
- Project Objectives
- Scope
- Functionality
- Solution
- Project Schedule
- Benefits
- Conclusions



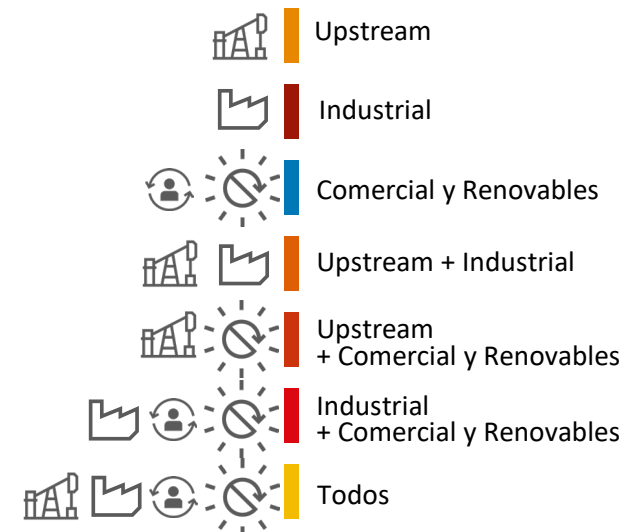
Introduction

Repsol 2022



Introduction

Repsol in the World



Introduction

APO Installed base at Repsol



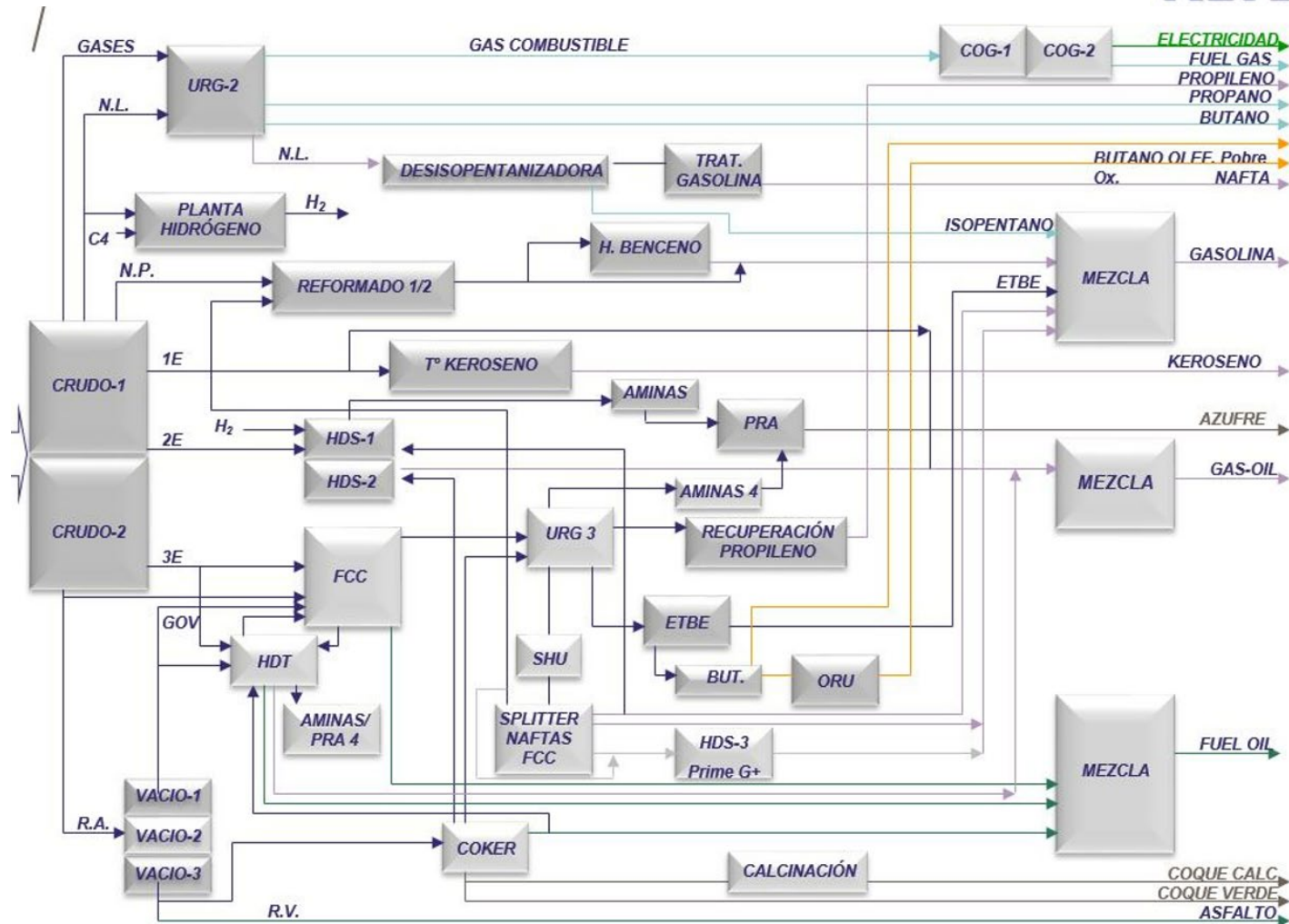
1. Cartagena (Spain) Refinery Hydrocracker Closed-Loop RTO (includes automatic LP Vector generation)
2. Tarragona (Spain) Refinery Hydrocracker Closed-Loop RTO (includes automatic LP Vector generation)
3. Tarragona (Spain) Refinery Multi-Unit CDU + VDU Closed-Loop RTO
4. Puertollano (Spain) Refinery Multi-Unit MHC + FCCU Closed-Loop RTO
5. **Coruña (Spain) overall Refinery Utilities Open-Loop RTO**
6. Coruña (Spain) Refinery Multi-Unit HDT + FCCU Closed Loop RTO
7. Petronor (Spain) Refinery Multi-Unit HDT + FCCU Closed Loop RTO
8. Pampilla (Peru) Refinery Multi-Unit CDU + VDU Closed-Loop RTO
9. Puertollano (Spain) Refinery Multi-Unit CDU-VDU Closed-Loop RTO
10. **Puertollano (Spain) overall Refinery Utilities Open-Loop RTO (in progress, commissioning Dec 2022)**



Introduction

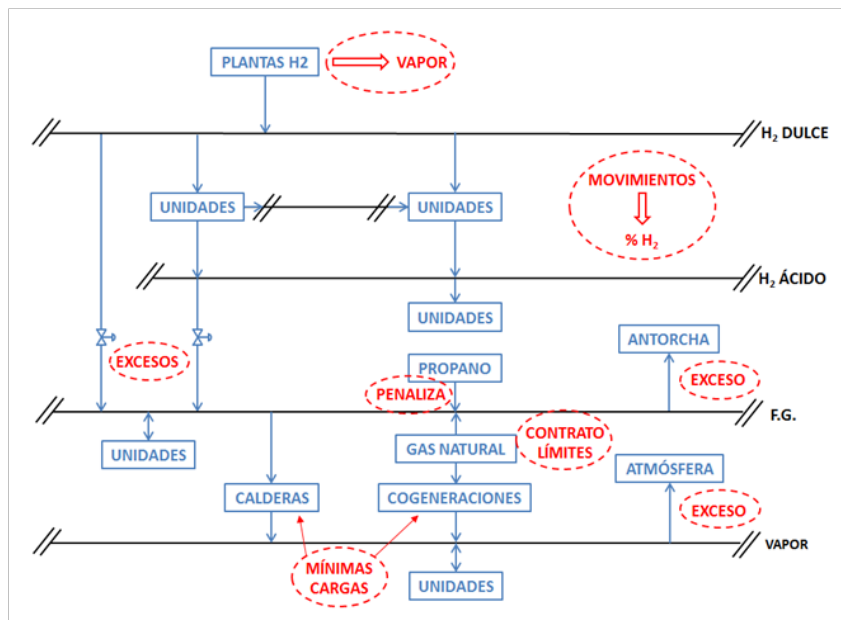
Coruña Refinery

- Location: The refinery is situated in the Bens Valley, about 3 km from the city and 5.5 from A Coruña port.
- Capacity: 5.5 million tons/annum & 120,000 bbl/day
- Refining Units
 - CDU - 120,000 bbl/day
 - VDU
 - Coker - 19,000 bbl/day
 - FCC
 - Hydrogen Plant
- Feedstocks:
 - Occasion Crudes
 - Vegetable Oils (into HDS and HDT)



Problem Description

Current Energy Management at Repsol Coruña



- Most of the changes in any utility (steam, FG, H2, electricity) impact in all the others.
- It is necessary to adjust the utilities continuously in any process side changes.
- Planning and programming does not consider the utilities.

+ H2

We normally produce more H2 than we really need

- We adjust minimum required purity
- Surplus transfer to FG
- Any increase/decrease impacts steam

+ Fuel gas

Punctual excesses

- FG sent to flare (on time)
- Actions are applied that usually lead to excess steam and unit de-optimizations
- Feed reduction to Platformers

+ Vapor

Steam venting

- There are deoptimizations to avoid venting
- If we minimize steam → we have more FG that is not consumed in boilers
- We hit minimum load in boilers or cogeneration

Project Objectives



- Monitoring and reduction of refinery's total energy and utilities costs
- Monitoring and optimization of CO2 emissions
- Balancing various the processes, utilities and energies costs:
 - H2
 - Natural Gas, Fuelgas, Fueloil
 - Steam
 - Electricity
 - Optimize relevant part of processes
- Generation of recommendations to the Utilities Shift Manager to reduce refinery's total energy and utilities costs at different levels of implementation
- Implementation of the "What if" tool to be used directly by the Utilities Shift Manager.



**Repsol Compromiso
Cero Emisiones Netas
2050**

Scope

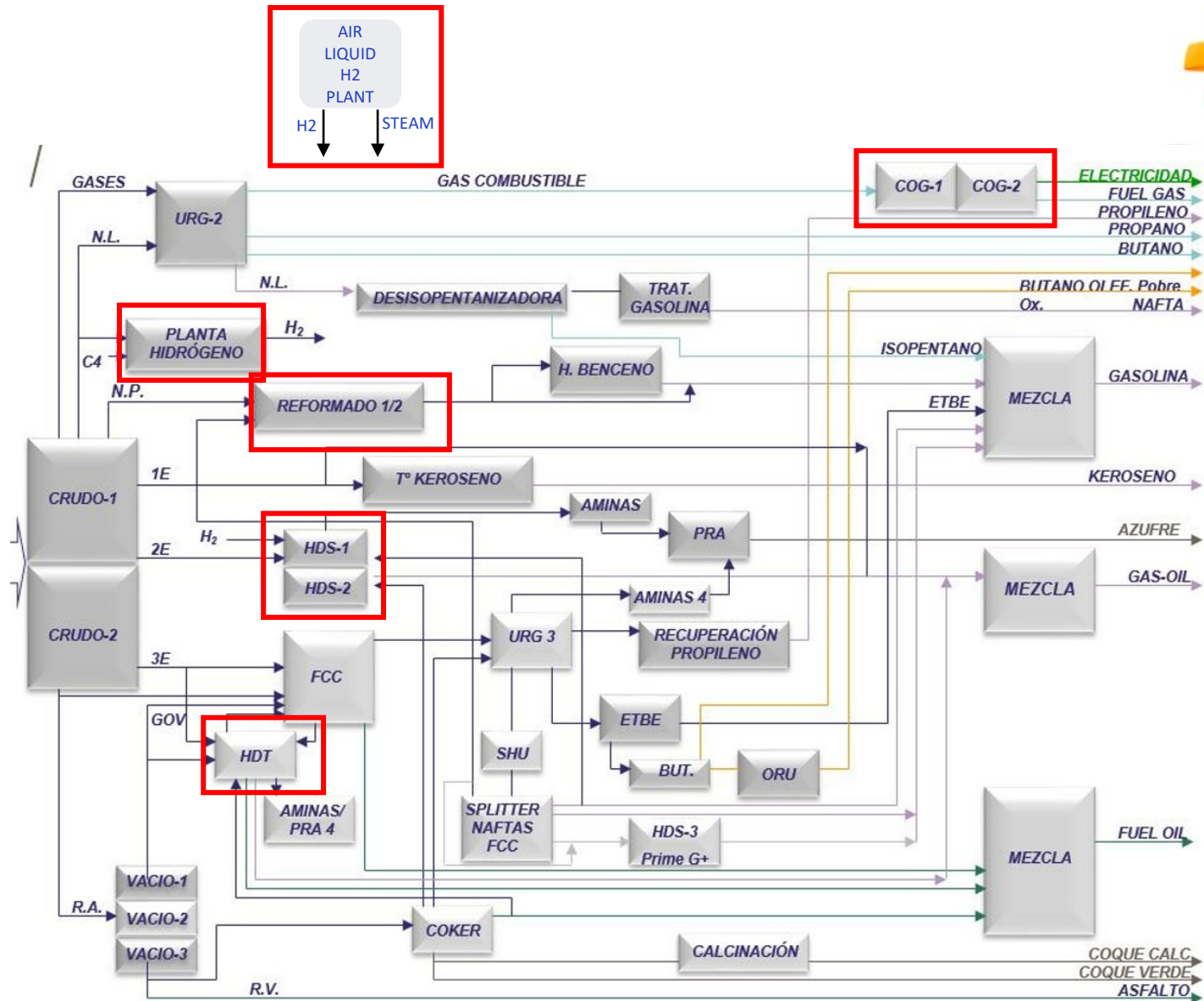


Process Units 1

- Steam and Power
 - 5 Steam Headers
 - 2 Cogen units – 1 with post combustion firing
 - 3 conventional boilers
 - Switchable electric motors / steam turbines between 4 levels
 - Steam Turbo generator
- Fuel Gas system
 - Refinery gases + NG import (pressure control) + Propane vaporizer
- H2 System
 - Import H2 & in house H2 steam reformer
 - 3 H2 headers
 - 2 Platformers
 - 3 major H2 consumers (2 HDS's and 1 HDT)
- Headers interactions:
 - Balanced FG with NG and LPG vaporization.
 - H2 bleeding to FG header
- Correlation models for HDT and Platforming
- Semi-rigorous models for HDS reactors for accurate calculation of H2 consumption and FG generation from different feedstocks.
- Simplified models of other refinery units for Fuel Gas/steam balance
 - Crude/ Vacuum Distillation units
 - FCC
 - Coker

Process side modelling

- Air Liquid H2 Plant: correlation H2 generated with steam provided to HPS.
- H2 Plant: : correlation H2 generated with steam provided to HPS and NG / FG consumed.
- HDT: correlation H2 consumed vs feed flowrate
- HDS1 & HDS2: H2 consumed vs feed composition & flowrate by means of simi-rigorous reactor model
- Platformer 2: correlation H2 & C1-C6 generation vs feed rate and output RON.



Scope

Features

- Steam /Electricity/Fuel (**complex contracts**)
 - Hourly electricity price, includes site electric balance and export limits
 - Natural gas price including contract penalties/ limits
- CO2 costs included – has important impact on optimization
- Propane & Butane cost included
- Boiler Feed Water (BFW) cost included
- H2 System
 - **Complex contract:** Import H2 price from Air Liquide (associated with steam), includes 2 tiers (pricing regimes)
 - H2 generation within refinery steam reforming plant included in model

- Constraints:
 - Operational constraints
 - Planning & logistic constraints

- Optimization Economic Objective function:
 - **Total utilities and energy cost = Fuels + Utilities + Electricity + CO2 emission**
 - Fuels: Fuel Oil / Natural Gas / LPG (Propane/Butane)
 - Utilities: H2/Steam/Water (BFW)
 - Electricity (Cogen, Turboalternator)



Functionality

Automatic Solution cases at each run (every hour)

Model includes 2 automatic optimize cases for current operation:

- **Case 1:** Easy to change equipment (mainly valves Ops, PID SetPoints,...)

- **Case 2:** More difficult to change that require several actions from operator, less frequent changes (mainly switchable motor/turbines, H2 from Air Liquide)

It shows clear actions for the Utilities Shift Manager with the economic impact of each.



Optimización - 2 Casos		Planta estable ✓ Online - 05/10/2022 08:26:34		<input type="checkbox"/> Límites <input checked="" type="checkbox"/> Delta Optimizar
				Optimizando Día 3
Acciones	Situación inicial	Caso 1 ✓	Caso 2 ✓	
▼ Vapor				
▼ Consumos				
Lam. 18 a 11	5,40 t/h 1,50 - 30,0	12,7 ▲ 7,30	12,0 ▲ 6,60	
▼ Turbinas				
Turb. 42 a 11 TipoB	13,6 t/h 0,00 - 43,6	13,6 0,00	13,4 ▼ -0,20	
▼ Beneficios		Caso 1 ✓ 47,6 €/h	Caso 2 ✓ 62,3 €/h	
▶ Vapor				
▶ H2				
▶ FG				
▼ Otros				
CO2 directo		15,9 €/h	20,8 €/h	
HDS1 producción LPG		-0,14€/h	0,12€/h	
HDS2 producción LPG		-0,51€/h	-1,17€/h	
Penalizaciones por venteos, antorcha, desoptimizaciones...		-14,3€/h	-5,81€/h	

Functionality



Automatic Solution cases at each run (every hour)

- *Two more cases are under development:*

- **Operational Case 3:** It optimizes the feed rates to HDS and Platformates taking into consideration the planned following 4 days (logistic constraints)

- **Planning Case:** it optimizes the programming plan for the 4 following days taking into consideration inouts from scheduler (planned crudes, vegetable oil processing,...).
 - Purpose: future operation could be infeasible / uneconomic. Allows current operation to adjustments to help and provides a view to the future utilities operation

Functionality

“What if cases” offline tool

- It allows the Utilities Shift Manager to run simulation “What-if” cases for planning on a Web terminal.
- System allows browsing through different datasets chronologically and select one to perform the simulation case.
- HMI allows the user to modify the model inputs for simulation.
- Examples: what if HDS units or benzene or butadiene units will be up/down in the coming days?.



Matrix

Simulación Modelo base: 18/07/2022 10:58:17

Variable a modificar	Unidades	Valor	L. Inf.	L. Sup.
VAPOR AP A TURBINA P-C2 (74FI0301.MC)		Valor simulado		
VAPOR AP A UNIDAD (13FI0297.MC)		Valor simulado		
VAPOR AP		Valor simulado		
VAPOR AP		Valor simulado		
VAPOR AP		Valor simulado		
VAPOR AP		Valor simulado		
VAPOR AP		Valor simulado		

Matrix

Simulación Modelo base:

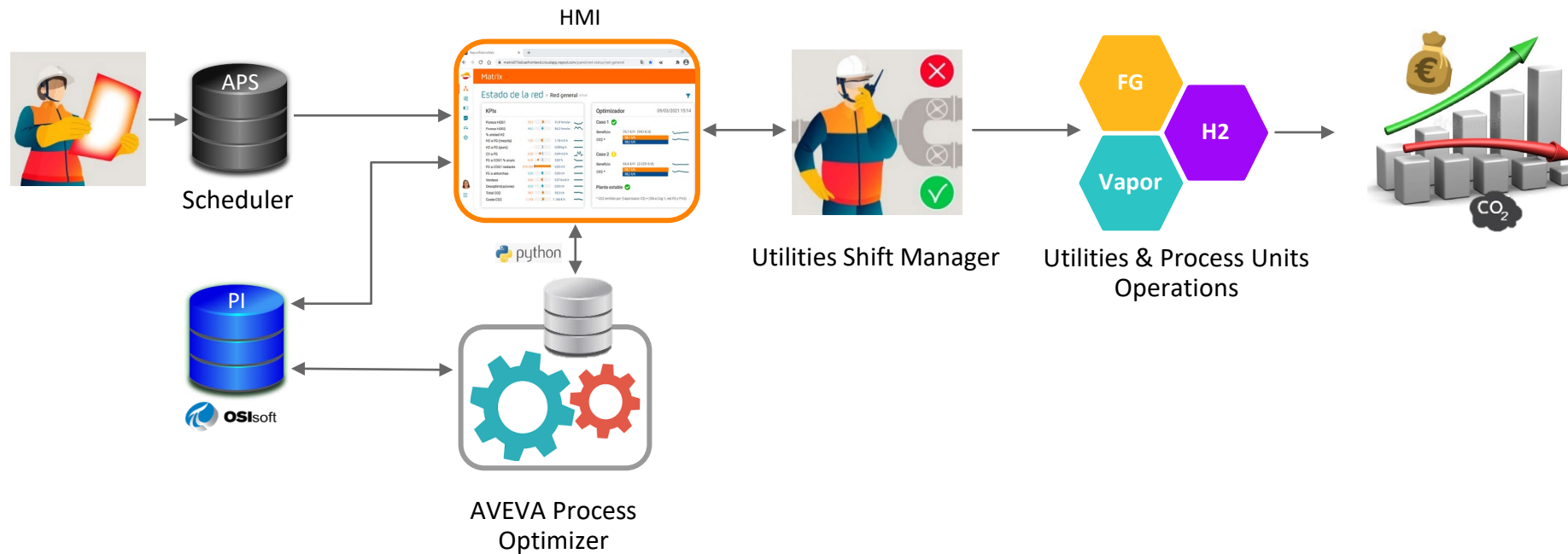
Variable a modificar	Unidades	Valor	L. Inf.	L. Sup.
Precio H2 de AL (MX.PRECIOH2AL)	€/t	2500	2.994	
Variable a modificar		Valor simulado		
Variable a modificar		Valor simulado		

☐ Delta

Acciones	Situación inicial	Simulado	Optimizado
Vapor			
Consumos			
V.B.P. a Tk's Nocturn	5,42 t/h	6,00 - 8,00	
V.B.P. a Tk's Bens	3,05 t/h	7,00 - 13,0	3,06 ▲ 0,01
Lam. 18 a 11	2,00 t/h	1,50 - 30,0	1,22 ▼ -0,78
Turbinas			
Turb. 42 a 11 TipoA	0,02 t/h	2,00 - 36,0	9,69 ▲ 9,67
Turb. 42 a 11 TipoB	9,61 t/h	0,00 - 43,6	9,67 ▲ 0,06
Turb. 42 a 4 TipoA	1,49 t/h	0,00 - 8,60	1,68 ▲ 0,19
Turb. 18 a 4 TipoA	16,0 t/h	0,00 - 25,0	- -
Turb. 18 a 4 TipoB	0,00 t/h	0,00 - 27,0	6,76 ▲ 6,76
Turb. 42 a 4 TipoB	14,1 t/h	5,00 - 72,4	14,0 ▼ -0,10

Repsol/AVEVA Solution

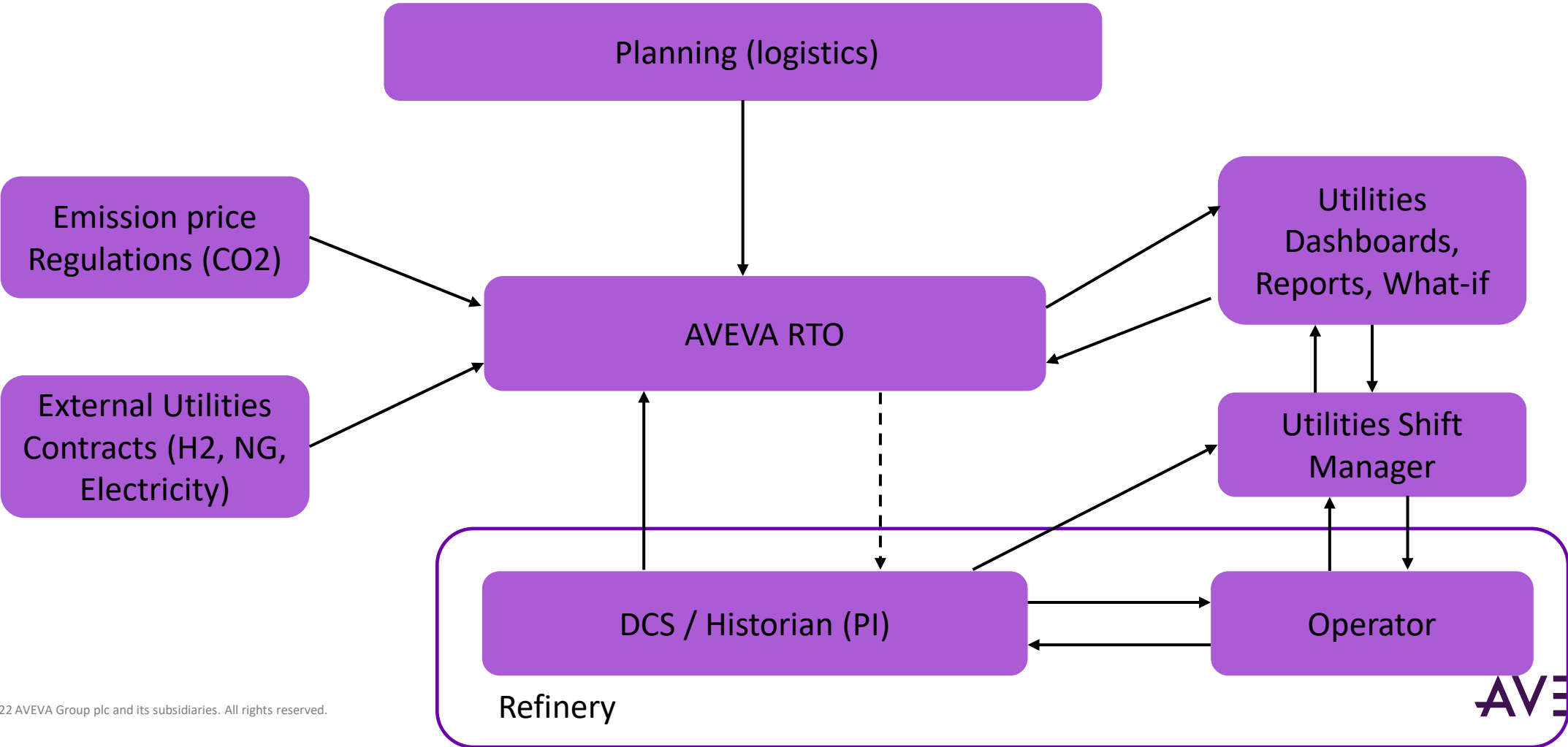
Open Loop Real Time Optimization



AVEVA Solution



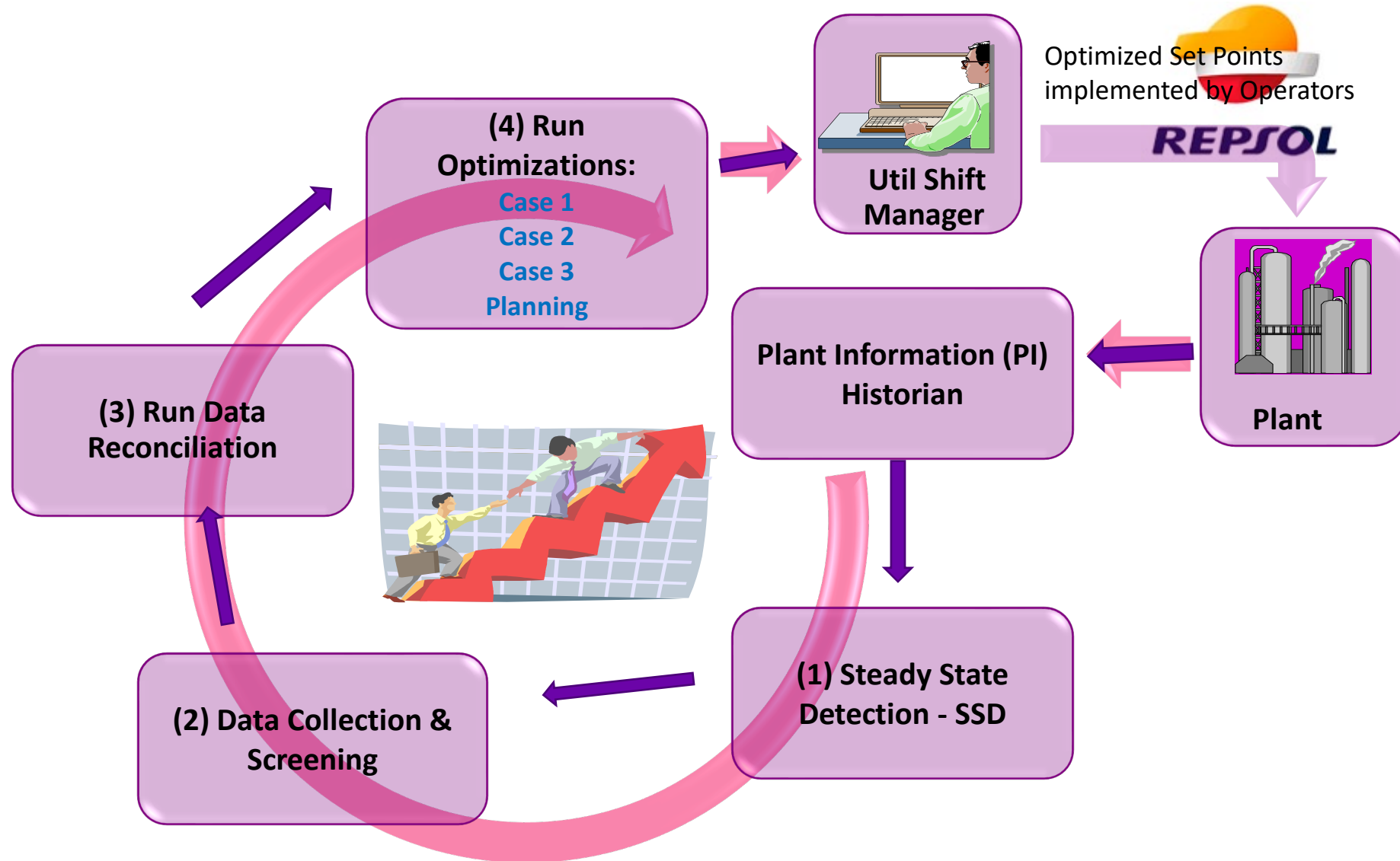
Information Flow



AVEVA Solution

Real Time System

- Open Loop – solution implemented by Utility Shift Manager.
- One solution per hour if steady state
- *Open or Closed Loop application based upon refinery policy.*
- This refinery choose open loop because:
 - Wide scope (H2/ steam/FG) therefore several consoles involved
 - Mixed slow and fast dynamics

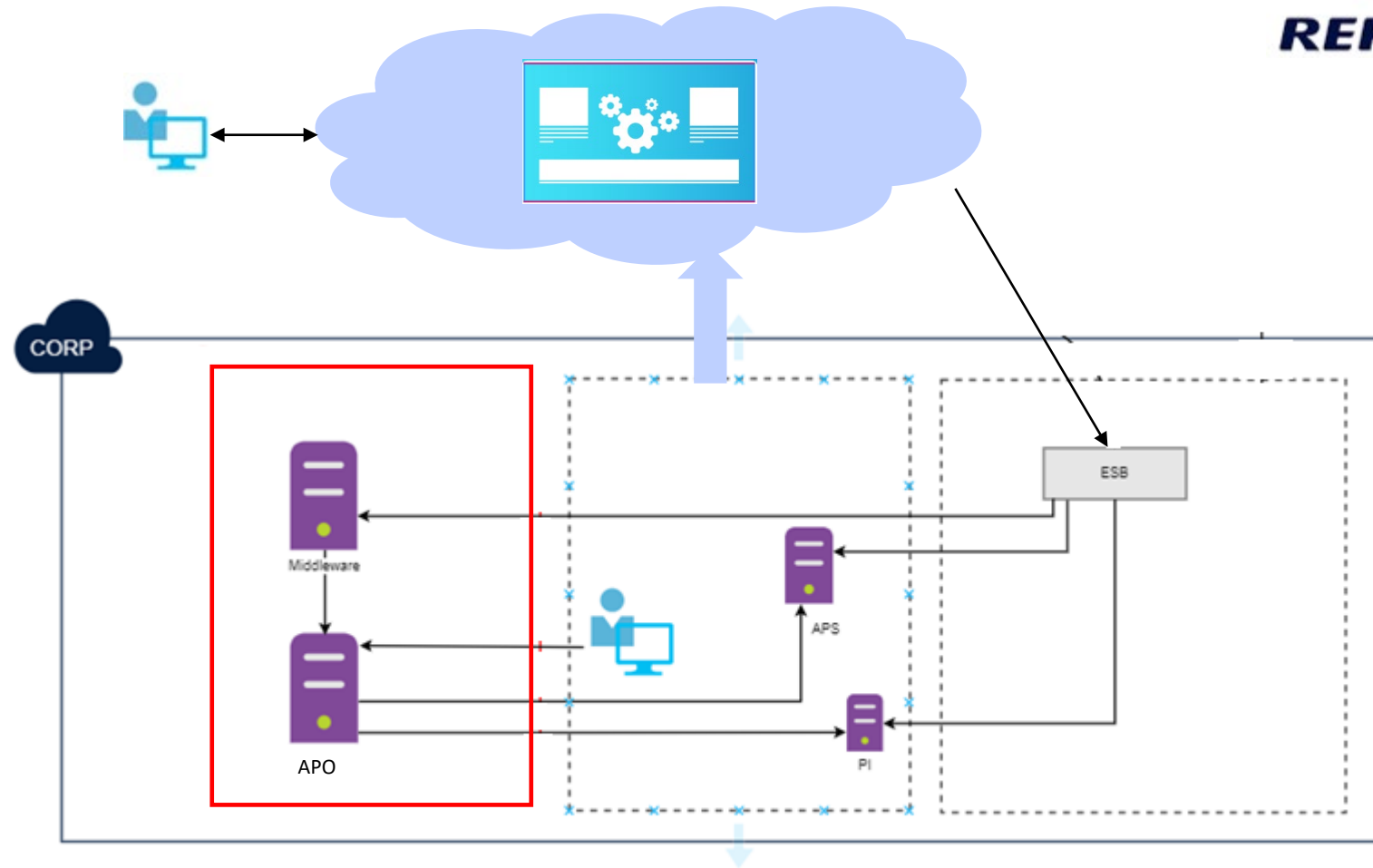


AVEVA Solution



Architecture

- APO running on premises in virtual environment.
- Visualization via Cloud in a Web terminal.
- Web terminal shows online results dashboards
- Web terminal includes HMI to use the offline “What if” cases tool.

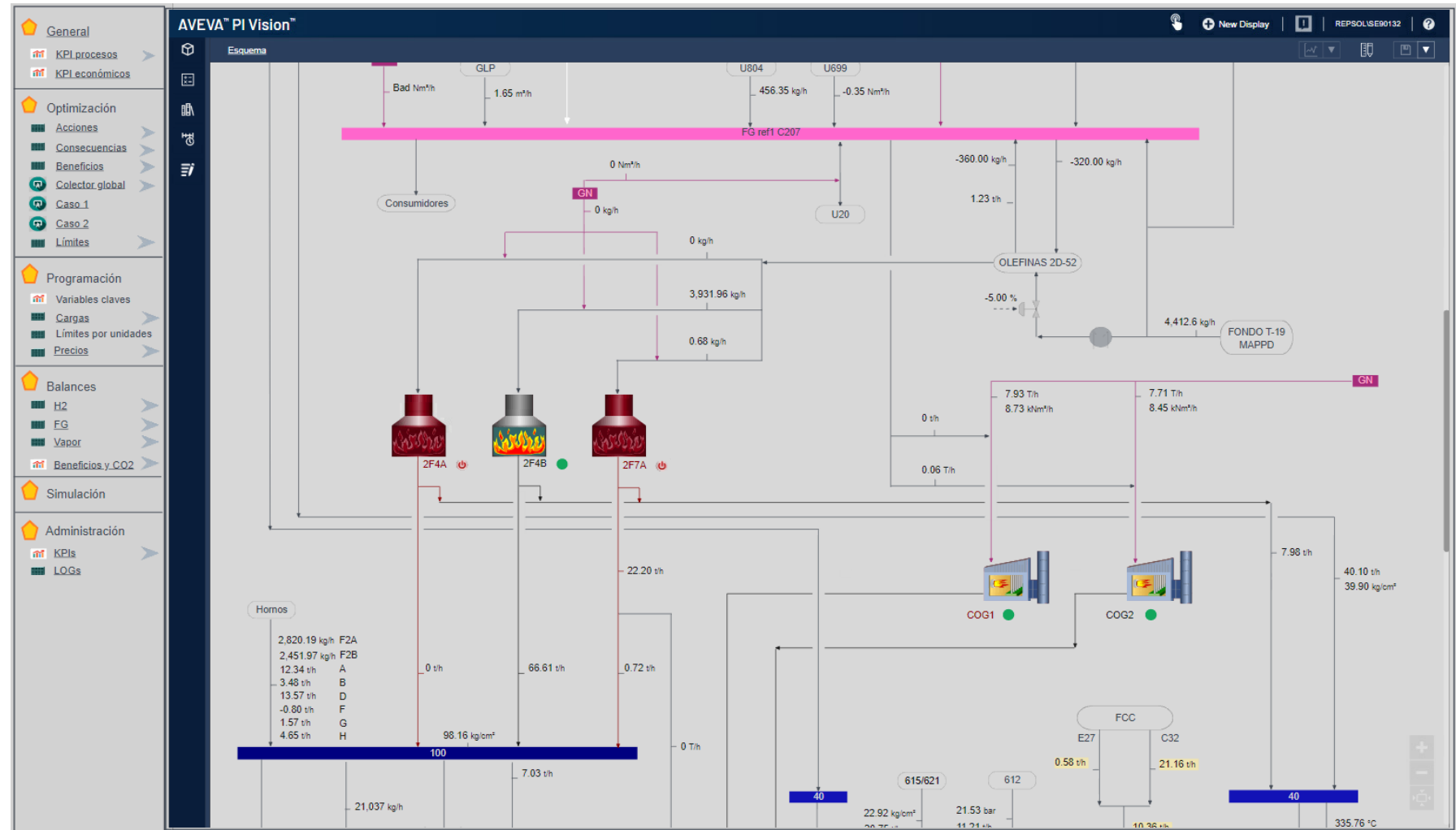


AVEVA Solution



PI Vision Visualization - Puertollano Refinery Deployment – FG & Steam interaction

- Comprehensive visualization of data from process (PI), planning, scheduler and optimizer from a Web terminal developed in **PI Vision**.
- User access authentication required
- Different levels of user access.



Project Execution Strategy



Requirements
Gathering and Design

Execution and Deployment

Warranty & Support

Phase-1 (1 month)

- Gathering Details
- Project Scope
- Functional Design
- Benefit Estimation



Phase-2 (9 months)

- Model Build
- Deployment at site
- Model validation
- Performance evaluation
- Commissioning



Phase-3 (1 Year)

- Continuous support
 - Model Convergence
 - Troubleshooting
 - Solution Analysis
- Enhancements/Modifications



Benefits



- Benefits of ROI less than 6 months.
- In 2021, 20% of the annual CO2 emission reduction due to all Repsol CO2 reduction technologies applied in Coruña Refinery was due to APO application.
- Benefit mechanisms:
 1. Reduce power generation during low electric price periods
 2. Reducing Letdown flows via better use of switchable turbines and demands
 3. Best use of discretionary steam production from process units
 4. Best use of Propane/Butane vs NG as marginal fuel
 5. Optimum dumping of H2 streams to Fuel Gas
 6. Optimum processing of high H2 consumption feeds
- Other benefits:
 - Learning of beneficial operations never thought about before by Utilities Shift Manager.
 - Accurate prediction of changes of energy, utilities and emissions (**CO2**) generated by the RTO
 - Evaluate of different operational strategies
 - Validation of the improvement of the refinery carbon footprint
 - Possibility to evaluate capital investment opportunities
 - Possibility to re-evaluate your utility contracts due to the agility provided by the tool.



Conclusions



- The close and continuous collaboration between Repsol Site and AVEVA team (as a single team) has guaranteed success delivering large carbon footprint reduction and large energy/utilities savings.
- Combination of AVEVA RTO and a comprehensive visualization tool (OsiSoft PI Vision) provides an efficient tool for optimal energy/utilities site operation.
- AVEVA RTO contributes greatly to achieve companies net-zero emission objectives.

Questions?

Please wait for the microphone.
State your name and company.



Please remember to...


Navigate to this session in the mobile
app to complete the survey.



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Over 20,000 enterprises in over 100 countries rely on AVEVA to help them deliver life's essentials: safe and reliable energy, food, medicines, infrastructure and more. By connecting people with trusted information and AI-enriched insights, AVEVA enables teams to engineer efficiently and optimize operations, driving growth and sustainability.

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