

OCTOBER 26, 2023

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# Hybrid Simulation with AI

James Kattapuram | R&D Director | Simulation

Jochen Steimel | R&D Product Owner | Simulation

JC Lee | Principal Engineer | Tech Support

David Smith | Principal AI Engineer | AVEVA AI CoE

**AVEVA**

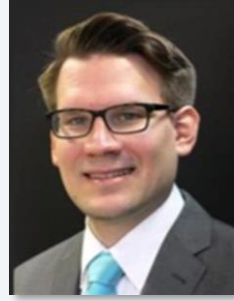


### **James Kattapuram**

**R&D Director Simulation Design Applications**

James holds a MS in Chemical Engineering from University of Southern California.

James has over 25+ years' experience in developing and leading Software R&D teams, to develop next generation Simulation, design and optimization applications.



### **Dr.-Ing. Jochen Steimel**

**Simulation Platform Partner Product Owner/ Architect**

Dr. Steimel holds a PhD in Chemical Engineering from TU Dortmund University.

In the first stop of his career, he worked at a German chemical company and was responsible for developing and maintaining an in-house simulator and was involved in digital/cloud/AI projects.

Since joining AVEVA, Dr. Steimel is developing the product vision for AVEVA Process Simulation (our next-generation simulation tool) and supports the R&D team with domain expertise.



### **Dr. JC Lee**

**Senior Principal Engineer**

Dr. Lee holds a PhD in chemical Engineering from Yonsei University in Korea.

He started his career as a process engineer at Daelim Engineering, a Korean EPC company, working on process design, simulation, EPC projects and developing licensing technologies.

Afterwards, He joined in SimSci division of Invensys and has contributed SimSci business at presale team and technical support team. He now leads APAC SimSci technical support team.



### **Dr. David Smith**

**Principal AI Engineer, AI Center of Excellence**

Dr. Smith is a Chartered Mechanical Engineer and holds a Ph.D. in Fluid Mechanics from Imperial College London

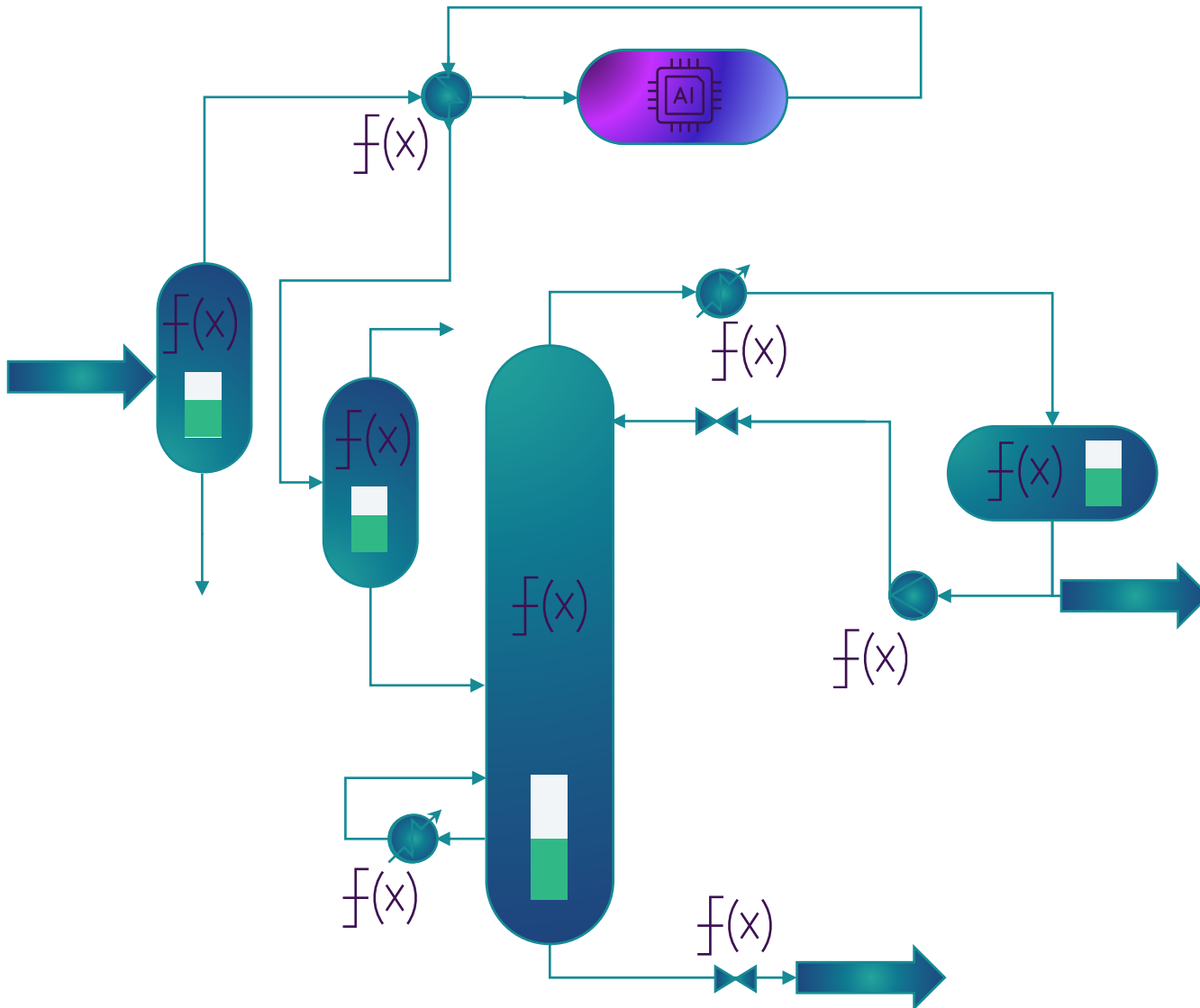
Spending the first half of his career in industry mainly with EPC companies; he led design, development, and commissioning of Power Plant processes and combustion systems. Moving to AVEVA, Dr. Smith joined the AI Center of Excellence, where his main activities are the integration of AI technologies with AVEVA's first principles simulation products for asset management and autonomous operations.

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# Agenda

- Introduction to Hybrid Modelling
- Hybrid Modelling in AVEVA™ Process Simulation 2023
- Lighthouse Customer Use Case: ISU Chemicals

# Hybrid Modelling



## Equation Based Model

Advantage
Accurate calculation of typical equipment
Prediction of untried operation
Acquisition of required data for design
Limitation
Difficult to obtain kinetic data for reaction
Need extra equation for special equipment
Limited by available thermodynamic properties data
Complex problems may be slow to converge

## ML Model

Limitation
Time consuming to generate model
Prediction within data range
Hard to calculate all required data for design
Advantage
Accurate reaction prediction from actual operating data
Prediction of any equipment by using actual operating data
Applicable for any properties from actual operating data
Can be faster to solve



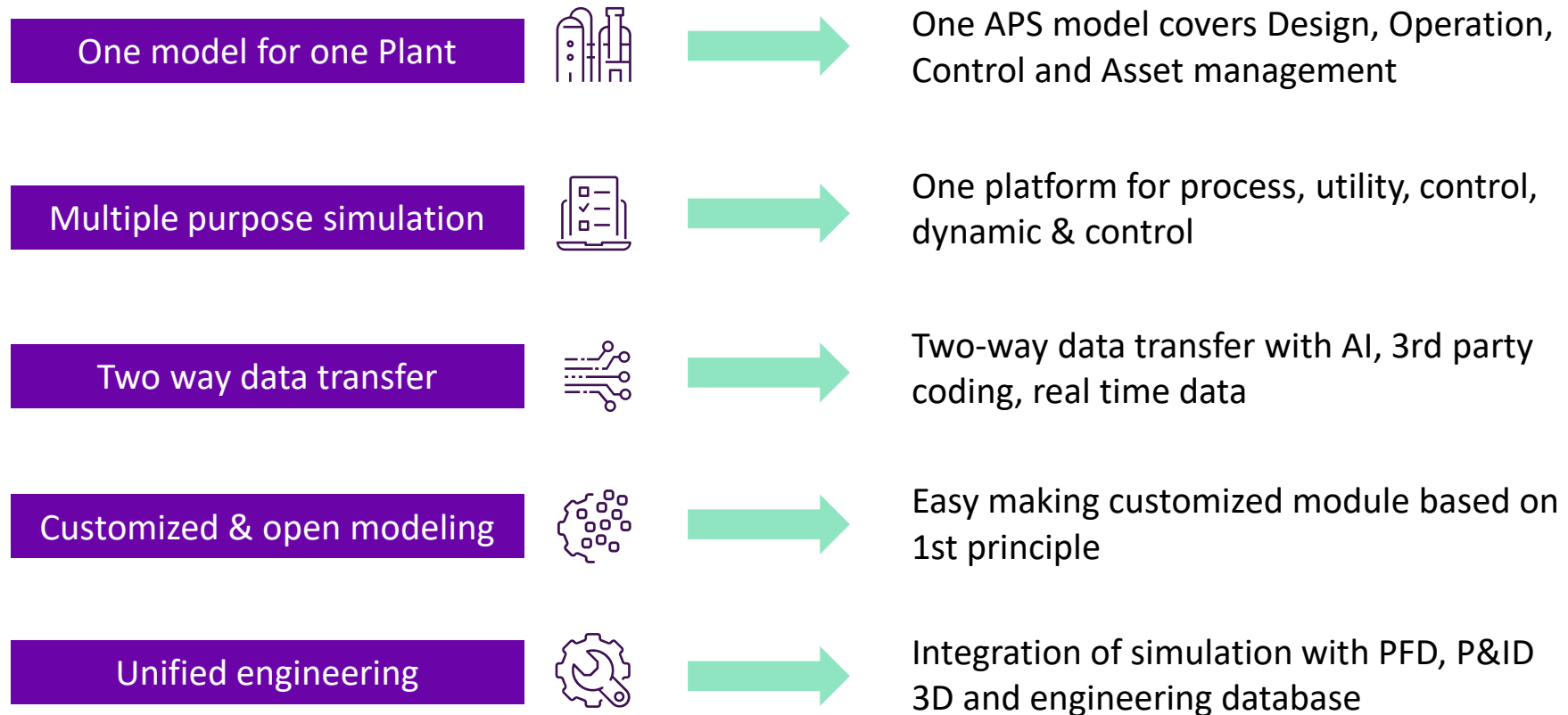
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# AVEVA™ Process Simulation

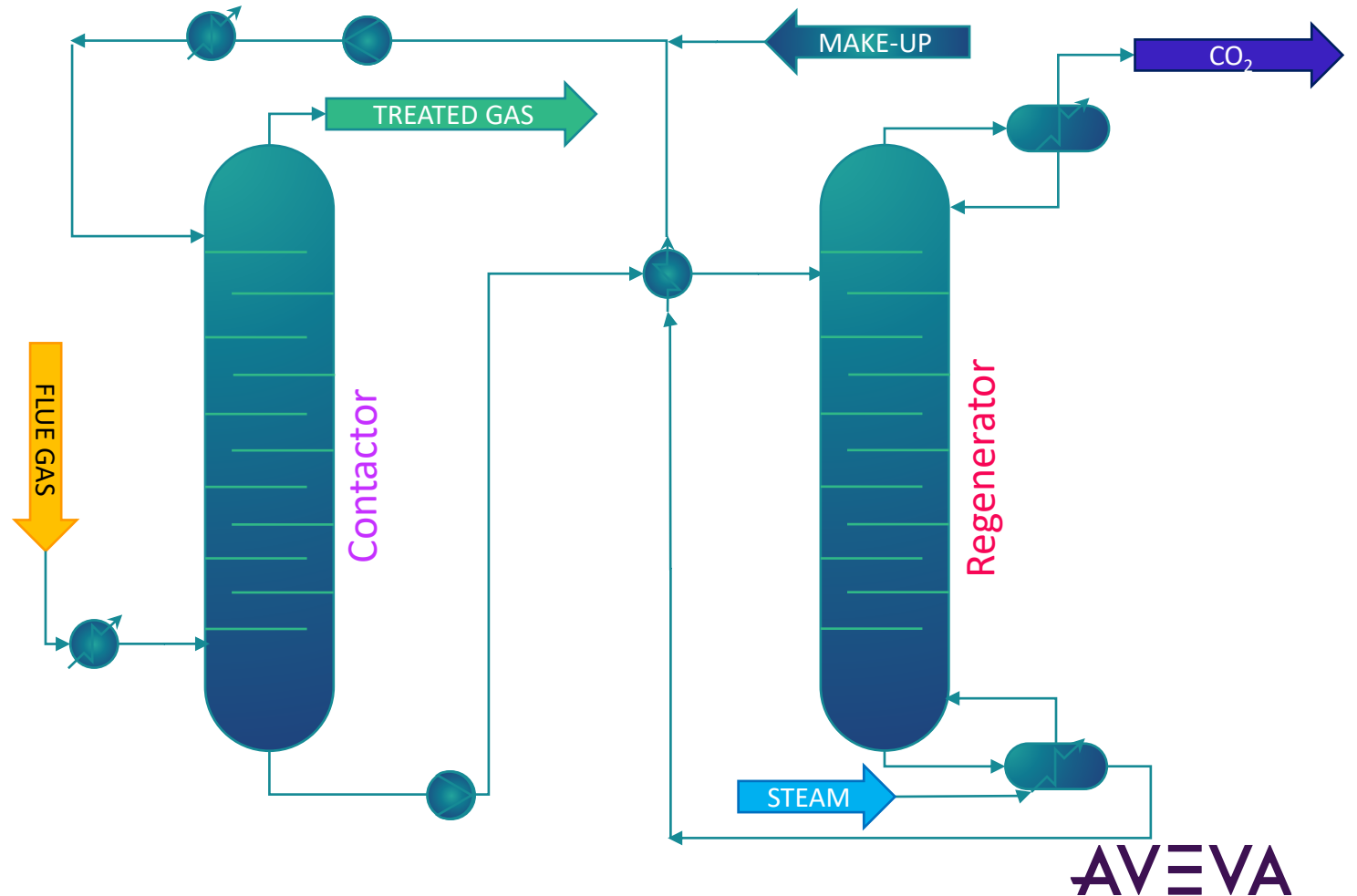
## State-of-the-Art Process Simulator



# Case Study

## Post Combustion Carbon Capture using Mono-Ethanol-Amine (MEA)

- Separate CO<sub>2</sub> from a **flue gas stream** coming from a combustion process
- MEA solution absorbs CO<sub>2</sub> in the **contactor**, in a **regenerator** the CO<sub>2</sub> is stripped and purified.
- Produces **Treated Gas** and **Pure CO<sub>2</sub>**
- Energy consumption (provided by **steam**) is very high
- APS model is relatively complex and takes 10-20 seconds to solve
- Goal to deliver a robust and fast ML model for the CCU process that can be appended to other models generating compatible flue gas streams

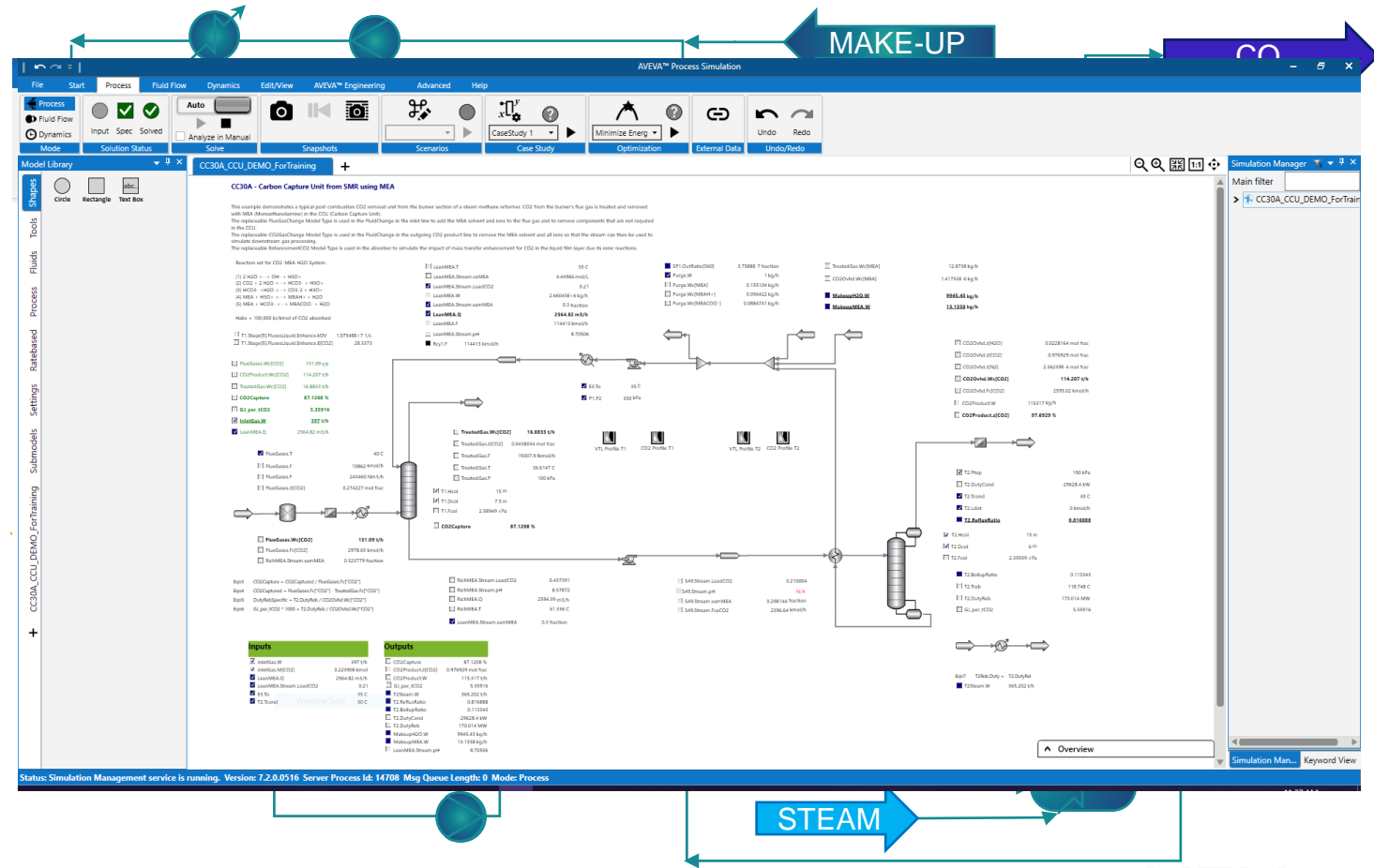




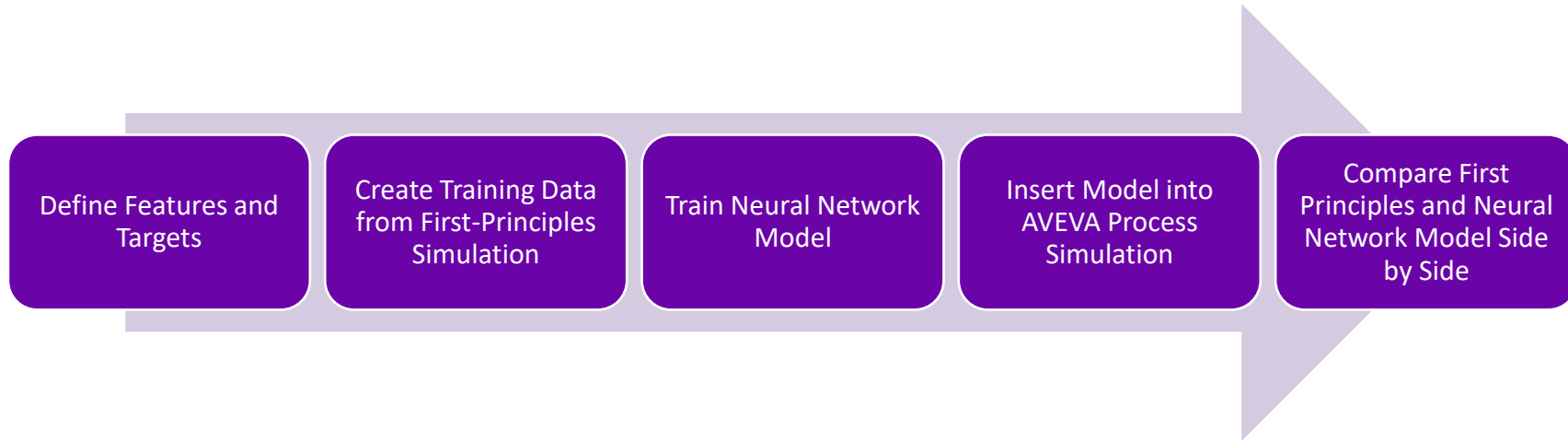
# Case Study

## Post Combustion Carbon Capture using Mono-Ethanol-Amine (MEA)

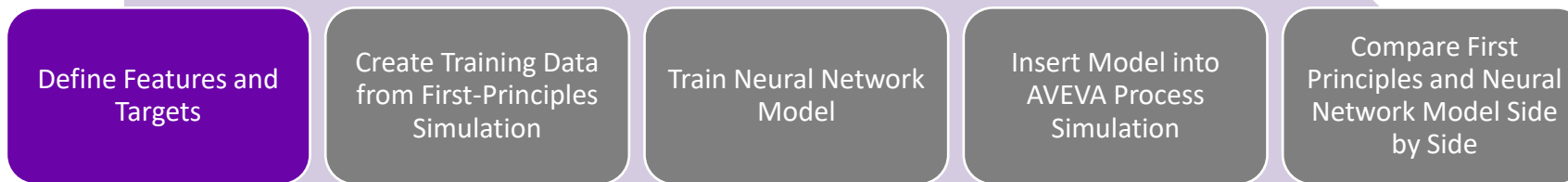
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# Approach

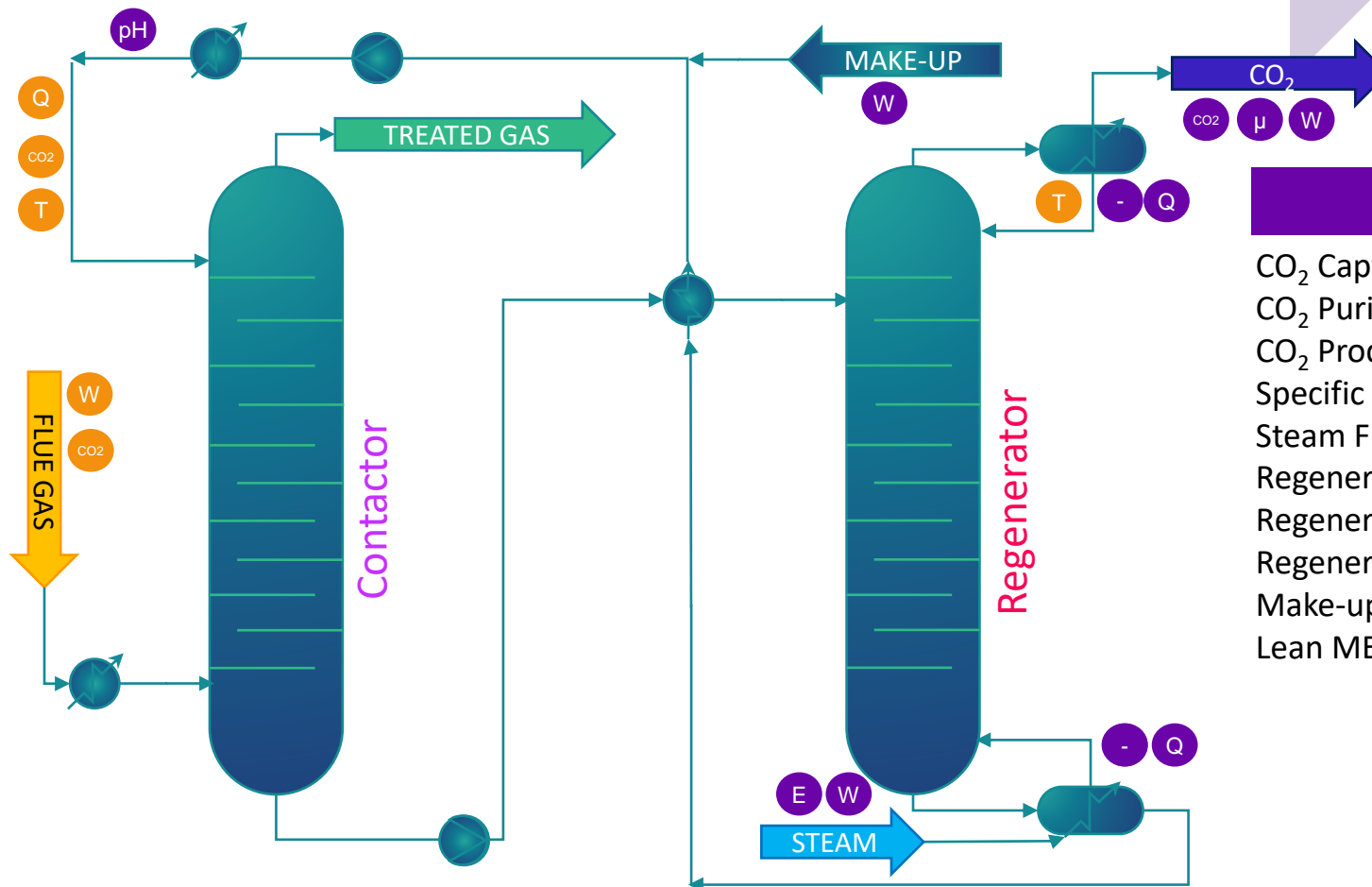


# Approach



## Features

- Flue Gas Mass Flow
- Flue Gas CO<sub>2</sub> Concentration
- Lean MEA Flow Rate
- Lean MEA CO<sub>2</sub> Load
- Lean MEA Temperature
- Regenerator Condenser Temperature

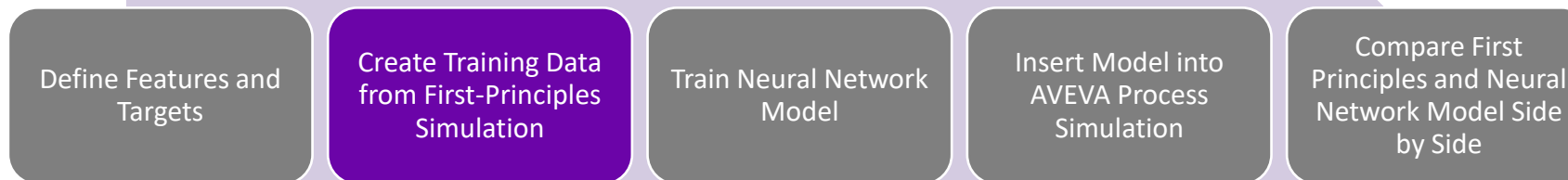


## Targets

- CO<sub>2</sub> Capture Efficiency
- CO<sub>2</sub> Purity
- CO<sub>2</sub> Product Flow
- Specific Energy Consumption
- Steam Flow
- Regenerator Reflux and Boil-up Ratios
- Regenerator Condenser Duty
- Regenerator Reboiler Duty
- Make-up Water and MEA
- Lean MEA pH

Carbonic acid

# Approach

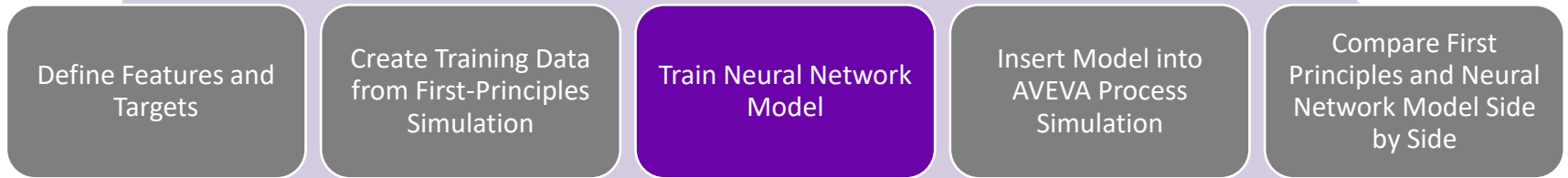


- APS scripting interface allows automated generation of training data from first principle model
- Random generation of Feature space using Latin-Hypercube sampling
- Repeat for 2000 cases

```
config_input= [
  {"Name": "Fluegas Mass flow", "SimName": "InletGas.W", "UOM": "t/h", "Min": 360.0, "Max": 440.0, "Nominal": 397.004},
  {"Name": "Fluegas CO2", "SimName": "InletGas.M[CO2]", "UOM": "", "Min": 0.1, "Max": 0.25, "Nominal": 0.22398},
  {"Name": "Lean MEA Flow rate", "SimName": "LeanMea.Q", "UOM": "m3/h", "Min": 2000.0, "Max": 2800.0, "Nominal": 2430.54},
  {"Name": "Lean MEA Flow CO2 Load", "SimName": "LeanMEA.Stream.LoadCO2", "UOM": "", "Min": 0.15, "Max": 0.3, "Nominal": 0.211278},
  {"Name": "Regenerator Condenser Temperature", "SimName": "E3.To", "UOM": "C", "Min": 25.0, "Max": 40.0, "Nominal": 30.0},
  {"Name": "Lean MEA T", "SimName": "T2.TCond", "UOM": "C", "Min": 35.0, "Max": 45.0, "Nominal": 40.0},
]

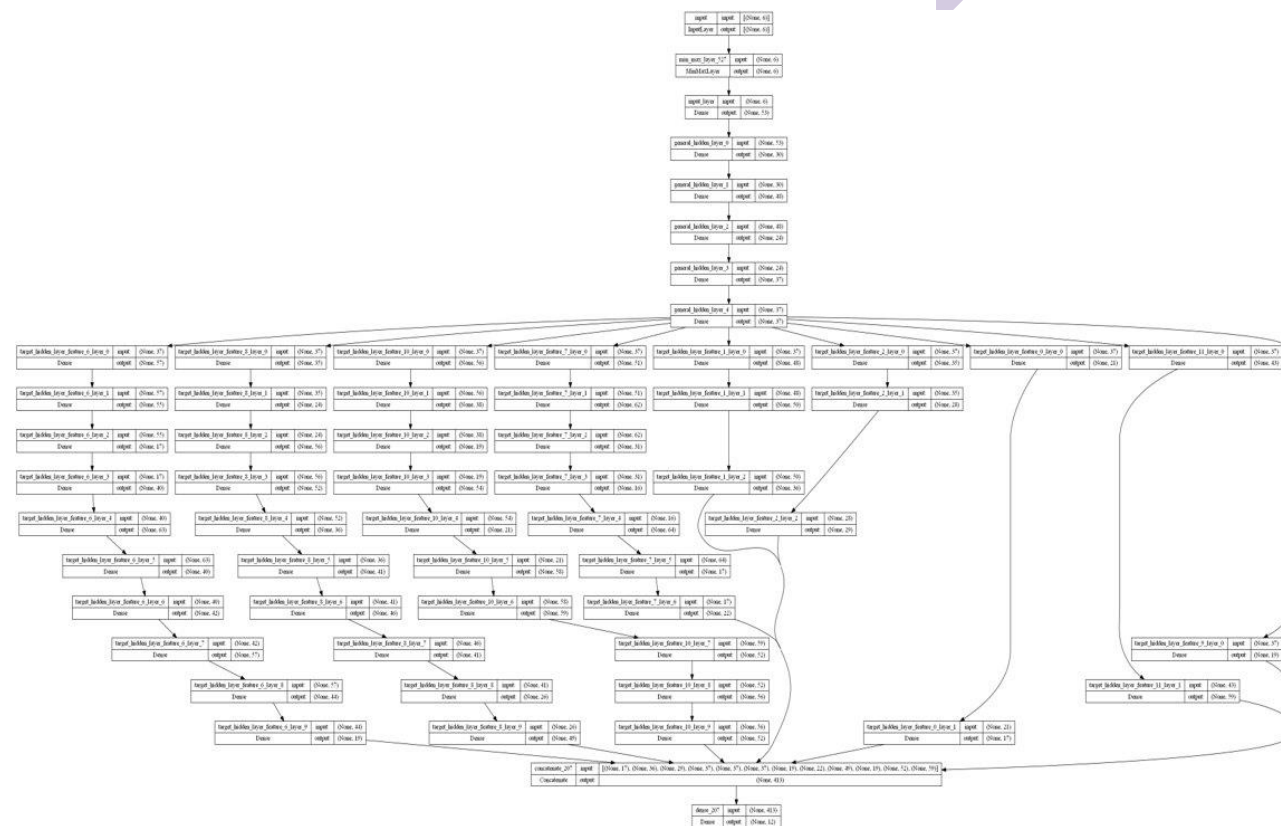
config_output= [
  {"Name": "CO2 Capture", "SimName": "CO2Capture", "UOM": "%", },
  {"Name": "CO2 Purity", "SimName": "CO2Product.z[CO2]", "UOM": "%", },
  {"Name": "CO2 Mass flow rate", "SimName": "CO2Product.W", "UOM": "t/h", },
  {"Name": "Specific Energy", "SimName": "GJ_per_tCO2", "UOM": "", },
  {"Name": "High Pressure Steam Flow rate", "SimName": "T2Steam.W", "UOM": "t/h", },
  {"Name": "Regenerator Reflux Ratio", "SimName": "T2.RefluxRatio", "UOM": "", },
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  {"Name": "Regenerator Condenser Duty", "SimName": "T2.DutyCond", "UOM": "MW", },
  {"Name": "Regenerator Reboiler Duty", "SimName": "T2.DutyReb", "UOM": "MW", },
  {"Name": "Makeup Water", "SimName": "MakeupH2O.W", "UOM": "kg/h", },
  {"Name": "Makeup MEA", "SimName": "MakeupMEA.W", "UOM": "kg/h", },
  {"Name": "Lean MEA pH", "SimName": "LeanMEA.Stream.pH", "UOM": "", },
]
]
```

# Approach

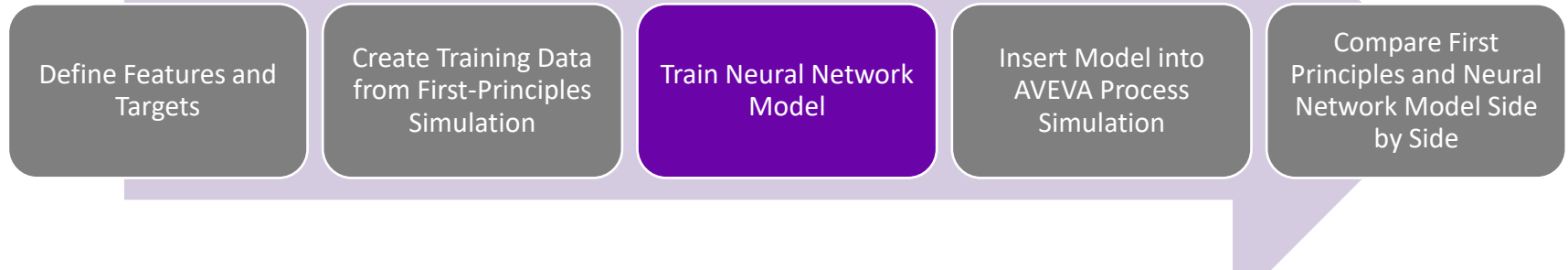


## ML Pipeline:

1. Scale features and targets
2. Optimise NN HPs and architecture
3. Train and Test



# Approach

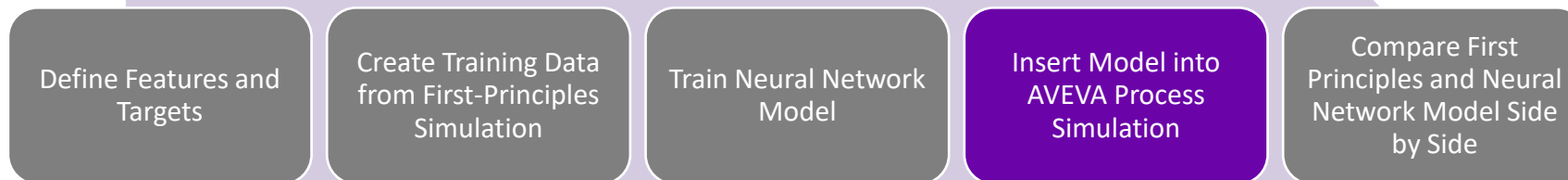


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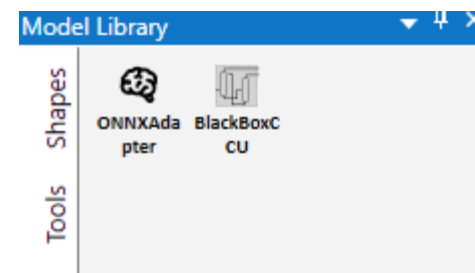


## Our Goals

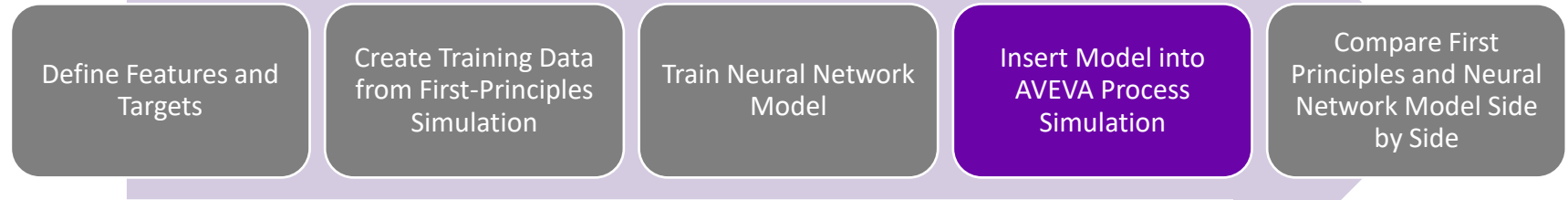
- Provide a single adapter in APS to cover a wide range of externally trained models
- Do not limit ourselves to a single ML pipeline frameworks (Tensorflow, pytorch, sklearn...)
- Do not try to reimplement a whole ML runtime engine
- Make it easy for the user to drag & drop a model on the canvas, provide some configuration and let them use the model immediately

## Our Approach

- Make use of ONNX (Open Neural Network eXchange)
  - Most pipelines provide a “toONNX” export
  - Microsoft provides open-source ONNX runtime in C#
- Encapsulate ONNX Runtime in an **External Equation Set**
- Call External Equation Set from a standard library model

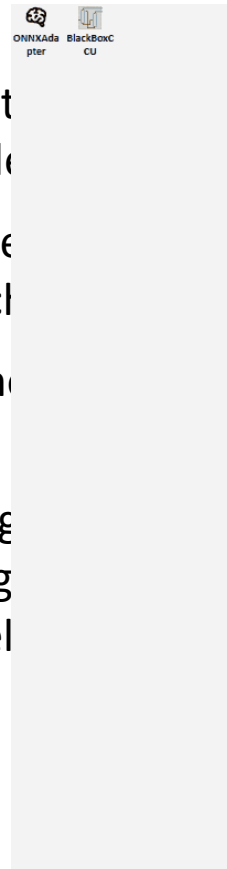


# Approach

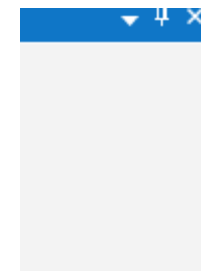


## Our Goals

- Provide a single adapter in APS to support a range of externally trained models
- Do not limit ourselves to a single framework (Tensorflow, pytorch)
- Do not try to reimplement a whole engine
- Make it easy for the user to drag and drop the canvas, provide some configuration so they can use the model immediately

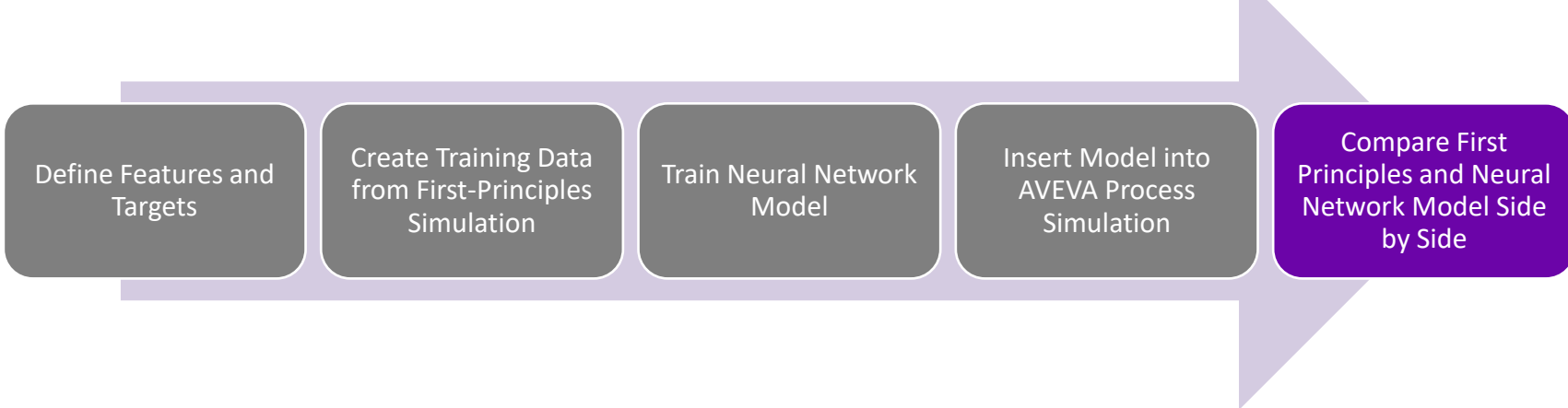


- Neural Network eXchange) to ONNX" export
- source ONNX runtime in C#
- use in an **External Equation**
- load from a standard library





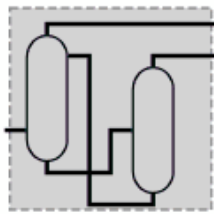
# Approach



## Linking Process Variables to the Black Box

<input checked="" type="checkbox"/> InletGas.W	380 t/h	<input checked="" type="checkbox"/> ML.Fluegas_W	380 t/h
<input checked="" type="checkbox"/> InletGas.M[CO2]	0.223908 kmol	<input checked="" type="checkbox"/> ML.Fluegas_M_CO2	0.223908 kmol
<input checked="" type="checkbox"/> LeanMEA.Q	2564.82 m3/h	<input checked="" type="checkbox"/> ML.LeanMEA_Q	2564.82 m3/h
<input checked="" type="checkbox"/> LeanMEA.Stream.LoadCO2	0.21	<input checked="" type="checkbox"/> ML.LeanMEA_CO2_Loading	0.21
<input checked="" type="checkbox"/> E3.To	35 C	<input checked="" type="checkbox"/> ML.LeanMEA_T	35 C
<input checked="" type="checkbox"/> T2.Tcond	30 C	<input checked="" type="checkbox"/> ML.Regenerator_T_Cond	30 C

- Eqn1 ML.Fluegas\_W = InletGas.W
- Eqn2 ML.Fluegas\_M\_CO2 = InletGas.M[CO2]
- Eqn8 ML.LeanMEA\_Q = LeanMEA.Q
- Eqn9 ML.LeanMEA\_CO2\_Loading = LeanMEA.Stream.LoadCO2
- Eqn10 ML.LeanMEA\_T = E3.To
- Eqn11 ML.Regenerator\_T\_Cond = T2.Tcond



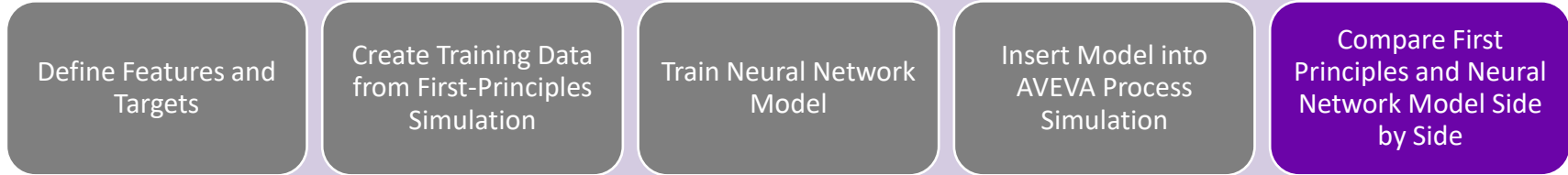
ML

## Comparison between Real Model and Surrogate Model

<input type="checkbox"/> CO2Capture	90.5531 %	<input type="checkbox"/> ML.CO2_Capture	92.178 %	<input type="checkbox"/> CO2Capture_Error	-1.79435 %
<input type="checkbox"/> CO2Product.z[CO2]	0.976926 mol frac	<input type="checkbox"/> ML.CO2_Purity	0.969279 mol frac	<input type="checkbox"/> CO2Purity_Error	0.782834 %
<input type="checkbox"/> CO2Product.W	114.728 t/h	<input type="checkbox"/> ML.CO2_W	119.29 t/h	<input type="checkbox"/> CO2W_Error	-3.9758 %
<input type="checkbox"/> GJ_per_tCO2	5.37531	<input type="checkbox"/> ML.Specific_Energy	5.21296	<input type="checkbox"/> SpecEnergy_Error	3.02029 %
<input checked="" type="checkbox"/> T2Steam.W	364.431 t/h	<input type="checkbox"/> ML.High_Pressure_Steam	375.128 t/h	<input type="checkbox"/> Steam_Error	-2.93508 %
				<input type="checkbox"/> <b>MAE</b>	<b>2.50167 %</b>

- Eqn12  $CO2Capture\_Error = (CO2Capture - ML.CO2\_Capture) / CO2Capture$
- Eqn13  $CO2Purity\_Error = (CO2Product.z[CO2] - ML.CO2\_Purity) / CO2Product.z[CO2]$
- Eqn14  $CO2W\_Error = (CO2Product.W - ML.CO2\_W) / CO2Product.W$
- Eqn15  $SpecEnergy\_Error = (GJ\_per\_tCO2 - ML.Specific\_Energy) / GJ\_per\_tCO2$
- Eqn16  $Steam\_Error = (T2Steam.W - ML.High\_Pressure\_Steam) / T2Steam.W$
- Eqn17  $MAE = (abs(CO2Capture\_Error) + abs(CO2Purity\_Error) + abs(CO2W\_Error) + abs(SpecEnergy\_Error) + abs(Steam\_Error)) / 5$

# Approach



**BlackBoxCCU1**

- BlackBoxCCU1.Fluegas\_W 397.004 t/h
- BlackBoxCCU1.Fluegas\_M\_CO2 0.22398 kmol
- BlackBoxCCU1.LeanMEA\_Q 2430.54 m3/h
- BlackBoxCCU1.LeanMEA\_CO2\_Loading 0.211278
- BlackBoxCCU1.Regenerator\_T\_Cond 30 C
- BlackBoxCCU1.LeanMEA\_T 40 C
- BlackBoxCCU1.CO2\_Capture 89.5903 %
- BlackBoxCCU1.Specific\_Energy 5.09775

**Optimization Set Editor**

Name: Minimize Specific Energy

Objective Function: Minimize BlackBoxCCU1.Specific\_Energy

Status	Name	Value	Lower Bound	Upper Bound	Units
●	BlackBoxCCU1.LeanMEA_Q	2430.54	2000	2800	m3/h
●	BlackBoxCCU1.Regenerator_T_Cond	30	25	40	C
●	BlackBoxCCU1.LeanMEA_T	40	35	45	C
●	BlackBoxCCU1.LeanMEA_CO2_Loading	0.211278	0.15	0.3	
●	BlackBoxCCU1.CO2_Capture	89.5903	85	100	%
●	BlackBoxCCU1.Specific_Energy	5.09775	1	10	

**Optimizer Log**

Optimizer started at 02/14/2023 14:14:38  
 Optimizer content for ONNX\_Blackbox\_Test  
 NonLinear Optimizer = Opera + Feasible Path.

Trace Level = 1  
 Max Optimization Iterations = 30  
 InitialHessianDiag = 1.0000E-06  
 ObjectiveTolerance = 1.0000E-02  
 ConstraintTolerance = 1.0000E-06

Opera Problem Summary

Number of Variables	= 14	Number of Objective Nonzeros	= 1
Number of Equalities	= 10	Number of Equality Nonzeros	= 28
Number of Inequalities	= 4		
Number of Inequalities	= 12		
Number of Complements	= 0		

Opera Iteration Summary

Iteration Number	Objective Value	Constraint Closure	Step Fraction	Active Bounds	Iteration Time
0	4.3168E+00	0.0000E+00		2	0.00
1	4.3165E+00	6.8780E-03	1.000E+00	2	0.00
2	4.3179E+00	6.0292E-14	1.000E+00	2	0.00
3	4.3173E+00	1.8102E-14	1.000E+00	2	0.00
4	4.3171E+00	1.6597E-10	1.000E+00	2	0.00
5	4.3169E+00	7.4685E-11	1.000E+00	2	0.00

The objective function was optimized! Returned code: 4

Optimizer result: Optimized  
 Optimizer ended at 02/14/2023 14:14:38

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# Agenda

- Introduction to Hybrid Modelling
- Hybrid Modelling in AVEVA™ Process Simulation 2023
- Lighthouse Customer Use Case: ISU Chemicals

# Isu Chemical predicts reactor yield to a 99.7% degree of accuracy

## Challenge

- Optimize reactor performance and establish a catalyst replacement plan
- Building Feed & Product component structure from sample assay data

## Solution

- Deployed a hybrid simulation of AVEVA™ Process Simulation and an AI reactor model to predict reactor yield and catalyst performance and decay

## Results

- **Reactor yield can be predicted on different recipes and operation environments by 99.7%**
- **It is possible to predict catalyst performance and establish an efficient plan for catalyst replacement.**
- **Engineers and operators can proactively simulate the plant through an external HMI built in Excel.**



“ [AVEVA Process Simulation] presents the very rigorous and powerful hybrid model combined with AI that can predict reaction yield, catalyst decay and operation performance”

DH Kim, Process Engineer, Isu Chemical

Interview with Professor Oh  
Responsible for ML model creation for ISU Chemicals Project



Hanbat National University, South Korea



# Takeaways

- ML models are highly promising for modelling processes where first principles models may lack accuracy or are slow to converge
- APS now has ML platform agnostic ONNX adaptor to run ML models within the APS flowsheet and generate hybrid grey box modelling
- ISU Chemicals is an early adopter and with Hanbat University already showed success with a challenging use case for reactor performance prediction

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AVEVA is a world leader in industrial software, providing engineering and operational solutions across multiple industries, including oil and gas, chemical, pharmaceutical, power and utilities, marine, renewables, and food and beverage. Our agnostic and open architecture helps organizations design, build, operate, maintain and optimize the complete lifecycle of complex industrial assets, from production plants and offshore platforms to manufactured consumer goods.

Over 20,000 enterprises in over 100 countries rely on AVEVA to help them deliver life's essentials: safe and reliable energy, food, medicines, infrastructure and more. By connecting people with trusted information and AI-enriched insights, AVEVA enables teams to engineer efficiently and optimize operations, driving growth and sustainability.

Named as one of the world's most innovative companies, AVEVA supports customers with open solutions and the expertise of more than 6,400 employees, 5,000 partners and 5,700 certified developers. The company is headquartered in Cambridge, UK.

Learn more at [www.aveva.com](https://www.aveva.com)